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Claims 1 - 20 canceled

21. (Currently amended) A method for in situ remediation of an aquifer having a treatment zone through which passes water contaminated with at least one chemical contaminant which method comprises:

injecting into the aquifer, by at least two conduits, an oxygen-containing gas at a pressure of at least 5 psig above the hydrostatic pressure at injection points; wherein the volume of oxygen-containing gas injected each time at each injection point contains from about 1 to about 100 times of minimum average volume (Vmin) in cubic feet of total oxygen, measured at ambient temperature and ambient pressure, Wherein Vmin can be calculated as:

V min=0.1 × A × B × P + N

Wherein

A = treated area (square ft)

B = treatment thickness (ft)

P = porosity

N = number of injection points

- 22. (Previously presented) The method according to claim 21, wherein the oxygen-containing gas is injected to the aquifer at a frequency of from about once a week to about ten times a day.
- (Previously presented) The method according to claim 21, wherein the injection oxygen-containing gas at each injection point lasts from about 0.05 to about 4 minutes;
- 24. (Previously presented) A method according to claim 21, wherein the oxygen-containing gas is injected to the aquifer by a plurality of gas injectors spaced less than 10 ft. apart.

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25. (Previously presented) The method according to claim 21, wherein injection frequency and volume at each injection point having the relationship according to the following equation:

Wherein:

e » natural exponential

V = volume of gas injected at each injection point (fi3)

F = frequency of injections (number of injections per day)

N = number of gas injection points

W = width of the treatment zone perpendicular to groundwater flow path (ft)

B = vertical thickness of treatment zone (ft)

Q = specific discharge of ground water to the treatment zone (fl/day)

H = Henry's Constant for contaminant of interest ((mg/L-water)/(mg/L-air))

- 26. (Previously presented) The method as claimed in claim 21, wherein the loss of contaminant(s) from volatilisation is less than 50% by weight.
- 27. (Currently amended) The method according to claim 21, wherein said contaminant is selected from the group consisting of (a) methyl-t-butyl ether (MTBE), (b) t-butyl alcohol (TBA), and (c) a mixture thereof; wherein at least a portion of the contaminant is degraded to carbon dioxide by said microbial culture.
- 28. (Previously presented) The method according to claim 21, wherein each injection of oxygen-containing gas at each injection point lasts from about 0.3 to about 2 minutes.

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29. (Currently amended) A method for in situ remediation of an aquifer having a treatment zone through which passes water contaminated with at least one chemical contaminant, which method comprises injecting into the aquifer, by at least two conduits, an oxygen-containing gas at a pressure of at least 5 psig above the hydrostatic pressure at injection points by pulsed injection at a frequency from about once a week to about ten times a day, wherein each injection of oxygen-containing gas at each injection point lasts from about 0.05 to about 4 minutes;

- 30. (Previously presented) The method as claimed in claim 29, wherein the loss of contaminant(s) from volatilisation is less than 50% by weight.
- (Currently amended) The method according to claim 29, wherein said contaminant is selected from the group consisting of (a) methyl-t-butyl ether (MTBE), (b)

t-butyl alcohol (TBA), and (c) a mixture thereof; wherein at least a portion of the contaminant is degraded to carbon dioxide by said microbial culture.

32. (Previously presented) The method according to claim 29, wherein each injection oxygen-containing gas at each injection point lasts from about 0.3 to about 2 minutes.

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33. (Previously presented) The method according to claim 29, wherein injection frequency and volume at each injection point having the relationship according to the following equation:

Wherein:

e = natural exponential

V = volume of gas injected at each injection point (fi3)

F = frequency of injections (number of injections per day)

N = number of gas injection points

W = width of the treatment zone perpendicular to groundwater flow path (ft)

B - vertical thickness of treatment zone (ft)

Q = specific discharge of ground water to the treatment zone (fl/day)

H = Henry's Constant for contaminant of interest ((mg/L-water)/(mg/L-air))

- 34. (Previously presented) The method of claim 32, wherein, $e^{i(-V \times F \times N \times B)/(W \times B \times Q)}$ is greater than 0.80.
- 35. (Previously presented) The method according to claim 11, wherein said contaminant is na oxygenate chemical, wherein $e^{i(-V \times F \times N \times 10)(W \times B \times Q)l}$ is greater than 0.90 and the contaminant loss from volatilization is less than 10% by weight.
- 36. (Currently amended) A method for in situ remediation of an aquifer having a treatment zone through which passes water contaminated with at least one chemical contaminant, which method comprises injecting into the aquifer, by at least two conduits, an oxygen-containing gas at a pressure of at least 5 psig above the hydrostatic pressure at

injection points with injection frequency and volume at each injection point having the relationship according to the following equation:

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Wherein:

e = natural exponential

V = volume of gas injected at each injection point (ft3)

F = frequency of injections (number of injections per day)

N = number of gas injection points

W = width of the treatment zone perpendicular to groundwater flow path (ft)

B = vertical thickness of treatment zone (ft)

Q = specific discharge of ground water to the treatment zone (ft/day)

H = Henry's Constant for contaminant of interest ((mg/L-water)/(mg/L-air))

- 37. (Previously presented) The method of claim 35, wherein, $e^{i(-V \times F + N \times 10)(W \times B \times Q)}$ is greater than 0.80.
- 38. (Previously presented) The method according to claim 35, wherein said contaminant is na oxygenate chemical; wherein $e^{g_* \cdot V \times F \times N \times H_2(W \times B \times Q))}$ is greater than 0.90 and the contaminat loss from volatilization is less than 10% by weight.